

Simulation of an Homogeneous Relaxation Model for a three-phase mixture

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Introduction

- Homogeneous relaxation model (HRM) for a three-phase flow with two miscible phases
 - ↪ Introducing the model
 - ↪ Numerical study of the convective part
 - ↪ Beginning of a numerical study of two source terms

Motivations : modeling of a water-vapor-gas flow which can appear during pressurized water reactor accident

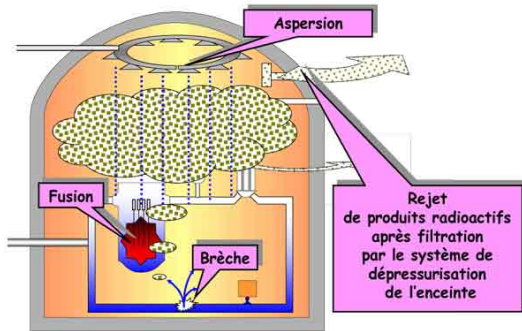


FIGURE – Loss of coolant accidents with primary failures in pressurized water reactor (IRSN)

Plan

- 1 Homogeneous relaxation model
- 2 Numerical study of the convective part
 - Schemes
 - Results
- 3 A study of two source terms
 - A first comparison
 - Γ_2 study for a two-phase flow model

Thermodynamical description

- Three phases who share the same velocity u : liquid water (l), vapor (v) and inert gas (g)
- ↪ Vapor and gas are totally miscible. Introducing mass fractions y_k , volume fractions α_k and energy fractions z_k , the intensive constraints are :

Intensive constraints

▶ Mass conservation : $1 = y_l + y_g + y_v$

▶ Energy conservation : $1 = z_l + z_g + z_v$

▶ Miscibility constraints :
$$\begin{cases} 1 = \alpha_l + \alpha_g \\ \alpha_v = \alpha_g \end{cases}$$

- Intensive description of a state : specific volume τ , internal energy e , gaseous mass fraction y_g and $Y = (y_l, \alpha_l, z_l, z_g)$ other fractions submitted to thermodynamics
- y_g is a constant since the gas is inert
- For a given state (τ, e, Y, y_g) , there must exist an unique Y_{eq} corresponding to the thermodynamic equilibrium, which only depends of (τ, e, y_g) and that maximises the entropy $\sigma = \sum_{k=l,g,v} y_k s_k$

Homogeneous relaxation model and its properties [O. Hurisse, L. Quibel, 2019]

[H. Mathis, 2019]

- HRM = Euler equations + advection on fractions, thermodynamics effects modeled by source terms Γ :

$$\begin{cases} \partial_t Y + u \partial_x Y = \Gamma \\ \partial_t y_g + u \partial_x y_g = 0 \\ \partial_t \rho + \partial_x \rho u = 0 \\ \partial_t \rho u + \partial_x (\rho u^2 + P) = 0 \\ \partial_t \rho E + \partial_x (\rho E + P) u = 0 \end{cases}$$

- $-\rho\sigma$ is a Lax entropy
- Hyperbolic system as long as the three phases are present
- ↪ System closed by given pressure laws and intensive constraints
- ↪ Source terms must satisfy the entropy growth according to the second law of thermodynamics
- Rankine-Hugoniot relations to build solutions of Riemann problems :

- ▶ Pressure and velocity conserved through contacts, not fractions

- ▶ Relations through shocks :

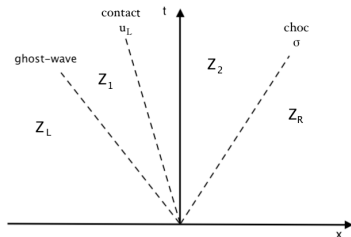
$$\begin{cases} [Y] = 0 \\ J = -\frac{[P]}{[u]} \\ J^2 = -\frac{[P]}{[\tau]} \\ [e] + [\tau] \frac{P_L + P_R}{2} = 0 \end{cases}$$

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Study framework

- Fractional step method :
 - ↪ Convective part solved with Finite Volume method :
VFRoe-ncv [T. Buffard, T. Gallouët, J.-M. Hérard, 2000]
Relaxation scheme [C.Chalons, J.-F. Coulombel, 2008]
 - ↪ ODE on source terms to take thermodynamics into account : $\dot{Y} = \Gamma(Y)$
- Equations of state :
 - ↪ 3 stiffened gas mixture (3 SG)
 - ↪ 2 SG + 1 NASG-CK law for liquid water (2 SG + 1 NASG-CK) [L. Quibel, 2020]
- Riemann problems structure : contact + shock



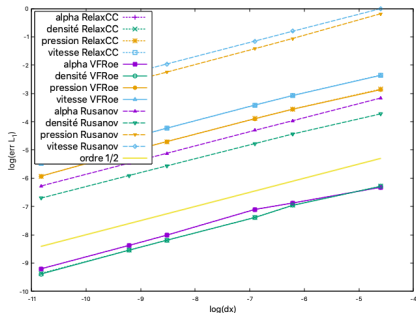
Objectives

Comparing VFRoe-ncv and relaxation schemes on atmospheric and high pressure Riemann problems.

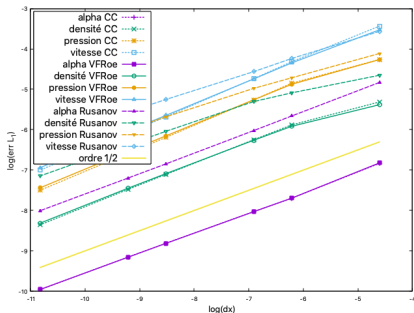
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Convergence results



(a) Atm. pressure Riemann problem

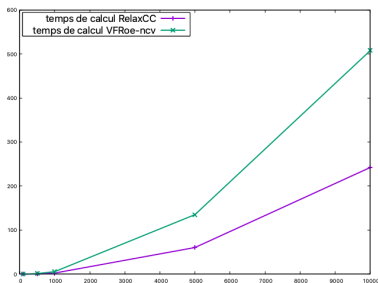


(b) High pressure Riemann problem

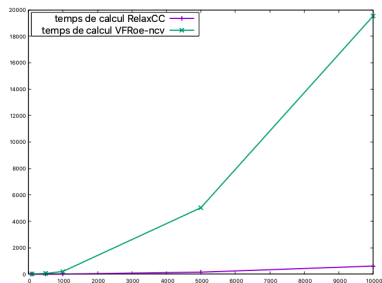
FIGURE – Finite volume schemes convergence curves for a 3 stiffened gas mixture.

- ~> Convergence rate of $\frac{1}{2}$
- ~> Very similar results between VFRoe-ncv and the relaxation scheme
 - Same type of results for a 2 SG + 1 NASG-CK mixture, but more implicate equations to solve, due to the implicit change of variables in the NASG-CK EOS.
- ~> Need to improve the robustness of some algorithms for VFRoe-ncv

VFRoe-ncv vs. relaxation scheme



(a) CPU time with respect to number of cells - 3 SG.



(b) CPU time with respect to number of cells - 2 SG + 1 NASG-CK.

FIGURE – Comparison of CPU time for each scheme.

- ↪ Relaxation scheme is much faster than VFRoe-ncv, since this last one does variable changes, and so implicit resolutions, at each cell. Consequently, the gap is wider for the more complex EOS mixture 2 SG + 1 NASG-CK.

Convective part conclusion

VFRoe-ncv and the relaxation scheme have similar errors, but the last one is faster and VFRoe-ncv has some lack of robustness.

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A first comparison

All of the following study is done for a 3 SG mixture. For relaxation time scales $\lambda > 0$, we consider :

$$\text{Type (1)} : \Gamma_1 = \lambda(Y_{\text{eq}} - Y)$$

- Very used model in homogeneous literature [O. Hurisse, 2014, 2017], [L. Quibel 2019]

- **Advantages :**

- ↪ Exact ODE solved for fixed time scales
- ↪ Simple trajectories

- **Drawbacks :**

- ↪ Computation of Y_{eq} that can be very hard depending of the choice of EOS [P. Helluy, L. Quibel 2019]
- ↪ Time scales constraints : they must be identical

$$\text{Type (2)} : \Gamma_2 = \lambda Y(1 - Y)\nabla_Y \sigma$$

- Recently introduced in homogeneous models [H. Mathis 2019], comes from full non-equilibrium models literature

- **Advantages :**

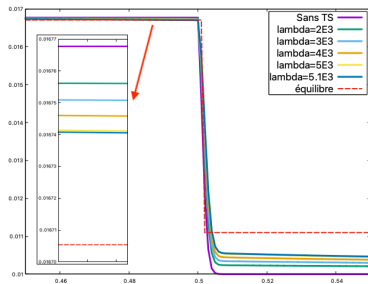
- ↪ No need to compute Y_{eq}
- ↪ Time scales can be different depending on fractions

- **Drawbacks :**

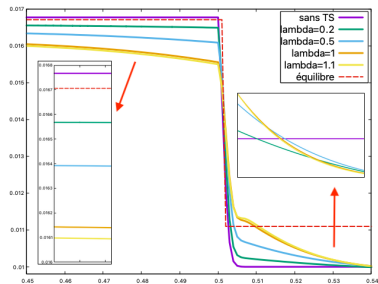
- ↪ Need a strong ODE solving method (implicit Euler scheme with Broyden algorithm)
- ↪ Far more complex trajectories, no longer monotonous

Coupling with the convective part

- We only consider common time scales according to fractions
- Convective part is solved by the relaxation scheme
- Γ_2 's ODE solved by an implicit Euler method



(a) α_l modification by Γ_1 .



(b) α_l modification by Γ_2

FIGURE – Atmospheric pressure Riemann problem modification by adding source terms for different time scales. Red dotted lines represents constant states equilibria.

- ↪ Monotonous evolution towards equilibrium for Γ_1 , non monotonous for Γ_2
- ↪ Limited choice of λ : algorithm fails due to non-admissible states around the contact

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Γ_2 study for a two-phase flow

- In order to simplify the analysis, we study these source terms for a two-phase flow. Thus, the ODE system is reduced to dimension 3 ($Y = (y_l, \alpha_l, z_l)$) that allows us to visualize data in space
- ↪ A first numerical study of trajectories brings us to consider $Y(1 - Y)\nabla_Y \sigma$ instead of $\nabla_Y \sigma$: solving is easier since $\forall t > 0, Y(t) \in]0; 1[$ ³
- ↪ Γ 's domain is a convex subset of the open cube, bounded by two planes that come from entropies definitions
- Important features :
 - ↪ Uniqueness of the inner equilibrium (up to now, lack of a concavity argument)
 - ↪ An equilibrium on the cube's border is necessary $0_{\mathbb{R}^3}$ or $1_{\mathbb{R}^3}$.

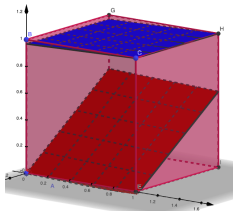


FIGURE – Γ 's definition domain for a given τ, e in space (y, α, z) .

Conclusions

- Two-parts numerical study
 - ↪ HRM convective part : efficient FV scheme
 - ↪ Source terms contribution : Γ_1 's limits could be avoided thanks to Γ_2

Forecast

- ↪ At-equilibrium Riemann problems
- ↪ Validation test cases
- ↪ Analysis of the two-phase source terms Γ_2

Thank you for your attention !